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WITH HEAT  
TRANSFER IN A  
VISCOUS  
INCOMPRESSIBLE  
FLUID BETWEEN TWO  
ROTATING DISKS IN  
THE PRESENCE OF  
INJECTION**

1958

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**Abstract**

**Full Text**

**FLUID MECHANICS**

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**UNSTEADY FLOW WITH HEAT TRANSFER  
IN A VISCOUS INCOMPRESSIBLE FLUID  
BETWEEN TWO ROTATING DISKS IN THE  
PRESENCE OF INJECTION**

*(Presented by Academician L. I. Sedov, 22 X 1957)*

1. Let us consider the problem of an unsteady flow of a viscous incompressible fluid, arising from a state of rest, between two infinite disks separated from one another by a distance  $h$ , of which one rotates with a time-dependent angular velocity  $\omega_0(t)$ , and the other with angular velocity  $\omega_1(t)$ . Let uniform injection of the same fluid take place from the first disk with a time-dependent velocity  $v_0(t)$ , and from the second with velocity  $v_1(t)$ .

If  $v_r, v_\theta, v_z$  are, respectively, the radial, tangential, and axial components of the velocity vector, then the boundary conditions of the problem, determined by the no-slip condition and by the presence of injection, and the initial conditions, determined by the absence of initial velocity of motion, are written in the form

$$v_r(r, 0, t) = v_r(r, h, t) = 0, \quad (1)$$

$$v_\theta(r, 0, t) = r\omega_0(t), \quad v_\theta(r, h, t) = r\omega_1(t); \quad (2)$$

$$v_z(r, 0, t) = v_0(t), \quad v_z(r, h, t) = v_1(t); \quad (3)$$

$$v_r(r, z, 0) = v_\theta(r, z, 0) = v_z(r, z, 0) = 0. \quad (4)$$

It is easy to verify that the Navier–Stokes equations, written in a cylindrical coordinate system, in the presence of axial symmetry and absence of body forces, and under conditions (1)–(4), admit the following solution:

$$v_r = \frac{r}{t_0} F(\zeta, \tau), \quad v_\theta = \frac{r}{t_0} G(\zeta, \tau), \quad v_z = \sqrt{\frac{\nu}{t_0}} H(\zeta, \tau),$$

$$P \frac{t_0}{\rho\nu} = \frac{1}{2} A(\tau) \frac{r^2}{\nu t_0} + B(\zeta, \tau), \quad \zeta = \frac{z}{\sqrt{\nu t_0}}, \quad \tau = \frac{t}{t_0}, \quad (5)$$

where  $t_0$  is a certain constant with the dimension of time,  $\nu$  is the coefficient of kinematic viscosity,  $P$  is the pressure, and  $\rho$  is the density.

In this case the functions  $F, G$ , and  $H$  must satisfy the system of nonlinear partial differential equations

$$\frac{\partial^4 H}{\partial \zeta^4} = H \frac{\partial^3 H}{\partial \zeta^3} + 4G \frac{\partial G}{\partial \zeta} + \frac{\partial^3 H}{\partial \zeta^2 \partial \tau}, \quad (6)$$

$$\frac{\partial^2 G}{\partial \zeta^2} = H \frac{\partial G}{\partial \zeta} - \frac{\partial H}{\partial \zeta} G + \frac{\partial G}{\partial \tau}, \quad 2F + \frac{\partial H}{\partial \zeta} = 0. \quad (7)$$

with the following boundary and initial conditions:

$$H(0, \tau) = \sqrt{\frac{t_0}{\nu}} v_0(t) = V_0(\tau), \quad H(\zeta_1, \tau) = \sqrt{\frac{t_0}{\nu}} v_1(t) = V_1(\tau); \quad (8)$$

$$\frac{\partial H}{\partial \zeta}(0, \tau) = \frac{\partial H(\zeta_1, \tau)}{\partial \zeta} = 0. \quad (9)$$

$$G(0, \tau) = \omega_0(t) t_0 = \Omega_0(\tau), \quad G(\zeta_1, \tau) = \omega_1(t) t_0 = \Omega_1(\tau), \quad (10)$$

$$G(\zeta, 0) = H(\zeta, 0) = 0, \quad \zeta_1 = \frac{h}{\sqrt{\nu t_0}}. \quad (11)$$

The functions  $A(\tau)$  and  $B(\zeta, \tau)$  are determined, after solving the problem (6)–(11), from the equations

$$A(\tau) = \frac{\partial^2 F}{\partial \zeta^2} + G^2 - F^2 - H \frac{\partial F}{\partial \zeta} - \frac{\partial F}{\partial \tau}, \quad \frac{\partial B(\zeta, \tau)}{\partial \zeta} = \frac{\partial^2 H}{\partial \zeta^2} - H \frac{\partial H}{\partial \zeta} - \frac{\partial H}{\partial \tau}.$$

Although the preceding arguments are valid for infinitely extended disks, the results obtained can be applied to disks of finite radius  $R$ , if this radius is large in comparison with the distance  $h$ . The resistance moments of disks  $M_0$  and  $M_1$ , with radii equal to  $R$ , will be

$$M_0(\tau) = -2\pi \int_0^R r^2 \tau_{z\theta} dr = -\frac{\pi \rho R^4}{2} \left( \frac{\nu}{t_0^3} \right)^{1/2} \frac{\partial G(0, \tau)}{\partial \zeta},$$

$$M_1(\tau) = \frac{\pi\rho R^4}{2} \left(\frac{\nu}{t_0^3}\right)^{1/2} \frac{\partial G(\zeta_1, \tau)}{\partial \zeta}. \tag{12}$$

2. It is known that the problem of heat transfer in a viscous incompressible fluid ( $\nu$ -const) can be solved after the dynamical problem has been solved.

It is easy to show that the unsteady energy equation, written in a cylindrical coordinate system, in the presence of axial symmetry,

$$\begin{aligned} & \rho c_v \left( \frac{\partial T}{\partial t} + v_r \frac{\partial T}{\partial r} + v_z \frac{\partial T}{\partial z} \right) = \\ & = \lambda \left( \frac{\partial^2 T}{\partial r^2} + \frac{1}{r} \frac{\partial T}{\partial r} + \frac{\partial^2 T}{\partial z^2} \right) + \\ & + A\mu \left\{ 2 \left( \frac{\partial v_r}{\partial r} \right)^2 + 2 \left( \frac{v_r}{r} \right)^2 + 2 \left( \frac{\partial v_z}{\partial z} \right)^2 + \left( \frac{\partial v_\theta}{\partial r} - \frac{v_\theta}{r} \right)^2 + \left( \frac{\partial v_\theta}{\partial z} \right)^2 + \left( \frac{\partial v_z}{\partial r} + \frac{\partial v_r}{\partial z} \right)^2 \right\}, \end{aligned} \tag{13}$$

where  $c_v$  is the specific heat at constant volume;  $\lambda$  is the coefficient of thermal conductivity;  $A$  is the thermal equivalent of mechanical energy, admits an exact solution in the form

$$T(r, z, t) = A \frac{\mu\nu}{\lambda t_0} \sum_{k=0}^n \left( \frac{r}{\sqrt{\nu t_0}} \right)^{2k} \Theta_{2k}(\zeta, \tau), \tag{14}$$

where  $n$  is an arbitrary integer, and the functions  $\Theta_{2k}(\zeta, \tau)$  ( $k = 0, 1, \dots, n$ ) must satisfy the one-dimensional heat-conduction equation with pere-

with variable coefficients, namely

$$\begin{aligned} & \frac{\partial^2 \Theta_0}{\partial \zeta^2} - \sigma \left( \frac{\partial \Theta_0}{\partial \tau} + H \frac{\partial \Theta_0}{\partial \zeta} \right) = -4\Theta_0 - 12F^2, \\ & \frac{\partial^2 \Theta_2}{\partial \zeta^2} - \sigma \left( \frac{\partial \Theta_2}{\partial \tau} + 2F\Theta_2 + H \frac{\partial \Theta_2}{\partial \zeta} \right) = -16\Theta_4 - \left( \frac{\partial G}{\partial \zeta} \right)^2 - \left( \frac{\partial F}{\partial \zeta} \right)^2, \\ & \frac{\partial^2 \Theta_4}{\partial \zeta^2} - \sigma \left( \frac{\partial \Theta_4}{\partial \tau} + 4F\Theta_4 + H \frac{\partial \Theta_4}{\partial \zeta} \right) = -36\Theta_6, \end{aligned} \tag{15}$$

.....

$$\frac{\partial^2 \Theta_{2(n-1)}}{\partial \zeta^2} - \sigma \left( \frac{\partial \Theta_{2(n-1)}}{\partial \tau} + 2(n-1)F\Theta_{2(n-1)} + H \frac{\partial \Theta_{2(n-1)}}{\partial \zeta} \right) = -(2n)^2 \Theta_{2n},$$

$$\frac{\partial^2 \Theta_{2n}}{\partial \zeta^2} - \sigma \left( \frac{\partial \Theta_{2n}}{\partial \tau} + 2nF\Theta_{2n} + H \frac{\partial \Theta_{2n}}{\partial \zeta} \right) = 0;$$

$$\sigma = \mu c_\nu / \lambda$$

is the Prandtl number.

Let us consider several boundary-value problems:

a) the case of a variable temperature along the radius of the disks:

$$\Theta_{2k}(0, \tau) = a_{2k}(\tau), \quad \Theta_{2k}(\zeta_1, \tau) = b_{2k}(\tau) \quad (k = 0, 1, \dots, n);$$

b) the case of variable heat fluxes along the radius of the disks:

$$\frac{\partial \Theta_{2k}(0, \tau)}{\partial \zeta} = c_{2k}(\tau), \quad \frac{\partial \Theta_{2k}(\zeta_1, \tau)}{\partial \zeta} = d_{2k}(\tau) \quad (k = 0, 1, \dots, n).$$

Here  $a_{2k}, b_{2k}, c_{2k}, d_{2k}$  ( $k = 0, 1, \dots, n$ ) are prescribed functions of  $\tau$ . In addition, the initial conditions must be satisfied:

$$\Theta_{2k}(\zeta, 0) = 0 \quad (k = 0, 1, \dots, n).$$

After the heat problem has been solved, the local Nusselt numbers  $N_0$  and  $N_1$  will be given by the formulas:

$$\frac{N_0}{\sqrt{\text{Re}}} = - \frac{\sum_{k=0}^n \frac{\partial \Theta_{2k}(0, \tau)}{\partial \zeta} \text{Re}^k}{\sum_{k=0}^n \Theta_{2k}(0, \tau) \text{Re}^k}, \quad \frac{N_1}{\sqrt{\text{Re}}} = \frac{\sum_{k=0}^n \frac{\partial \Theta_{2k}(\zeta_1, \tau)}{\partial \zeta} \text{Re}^k}{\sum_{k=1}^n \Theta_{2k}(\zeta_1, \tau) \text{Re}^k},$$

where

$$\text{Re} = \frac{r^2}{\nu t_0}, \quad N_0 = \frac{-\lambda \left. \frac{\partial T}{\partial z} \right|_{z=0} r}{\lambda(T - T_0)}, \quad N_1 = \frac{\lambda \left. \frac{\partial T}{\partial z} \right|_{z=h} r}{\lambda(T - T_0)},$$

$T_0$  is the characteristic temperature.

The solution obtained is exact in the sense that equations (6), (7), and (15) can be solved, for example, by a numerical method.

Received  
1 X 1957

*Note: Figure translations are in progress. See original paper for figures.*

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